



# Deposit Removal Current Technology & Challenges

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Clyde Industries



# Deposit Removal

## Three Objectives

Don't Plug & Damage	Don't plug and/or damage my boiler
Don't waste	Don't waste my steam
Safe & Reliable	Keep it Safe & Reliable

## Technology Development

- Pulsating Jets
- Nozzle Separation Distance
- Leading Edge Nozzle
- Fully Expanded Nozzle
- Targeted / Intelligent Sootblowing
- Zero Cooling Flow
- 9-14 bar Low Pressure Sootblowing
- Lance Design
- Carriage Fail Safe Design
- Fitness to Operate Sensors

# Pulsating Jet & Nozzle Distance

## • University of Toronto Research Consortium

### 6. Effect of Jet Characteristics on Removal of Cylindrical Brittle Deposits

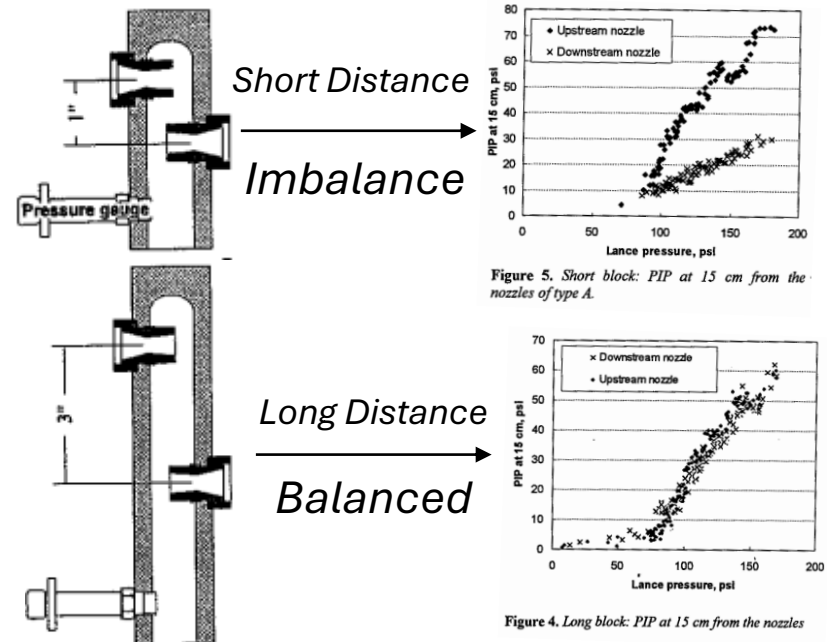
Morteza Eslamian, Ameya Pophali, Donald Cormack, and Honghi Tran

breakup. When a single pulse jet (fast sootblowing) was used, only 20% of model deposits broke. In the case of a pulsating jet (fast and frequent sootblowing), all deposits broke and when a continuous jet was employed, 60% of deposits broke. Since the deposits made with  $\eta = 1.5$  were breakable only at 5 cm, it was not possible to produce graphs similar to those for the soft deposits ( $\eta = 2$ ).

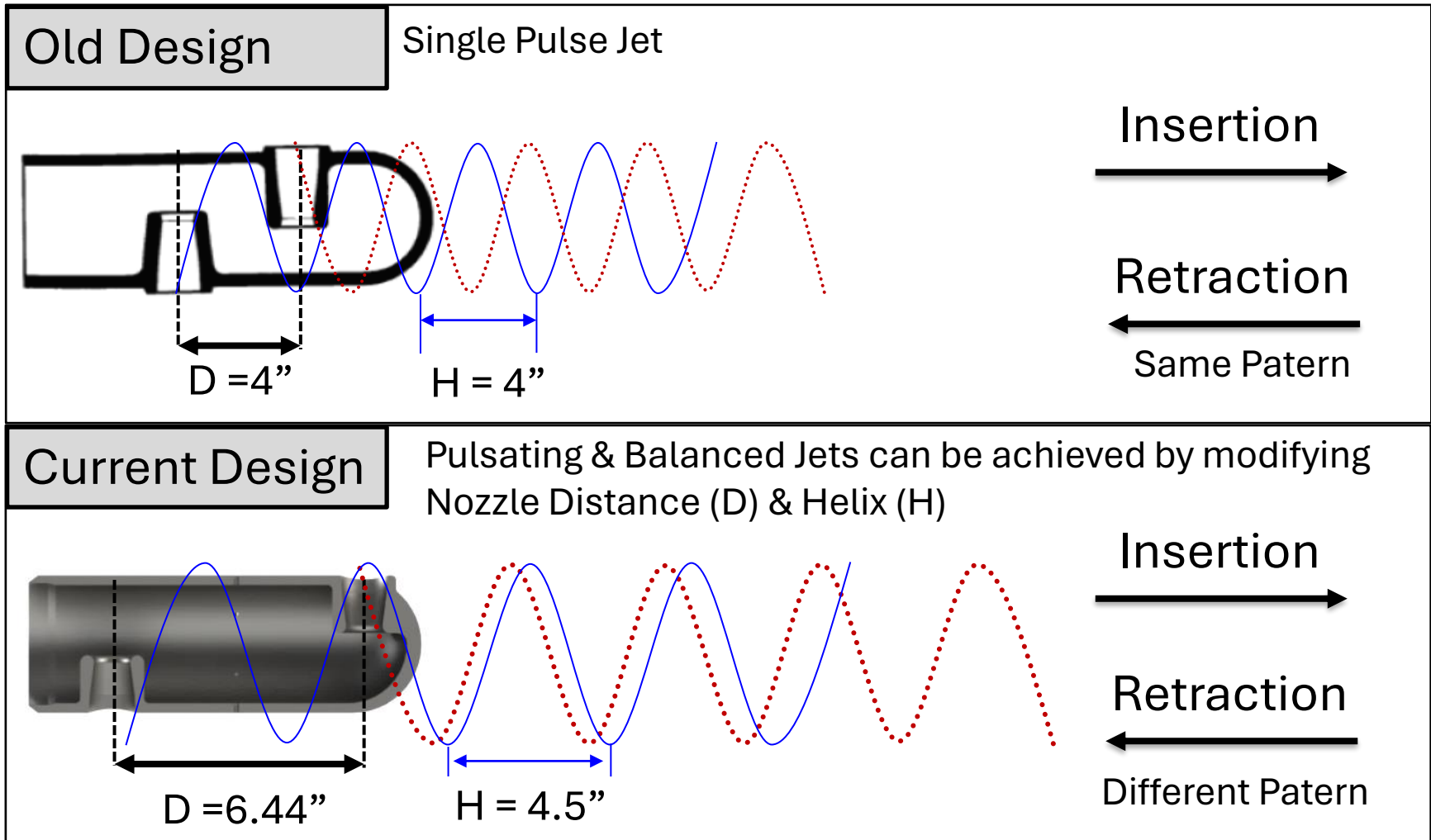
- Single pulse jet : 20% deposits removed
- Pulsating Jet : 100% removed
- Continuous Jet : 60% removed

### 11. Effects of Nozzle Arrangement on Jet Propagation Part II: Two Nozzle Tests

Andrei Kaliazine, Donald E. Cormack and Honghi Tran



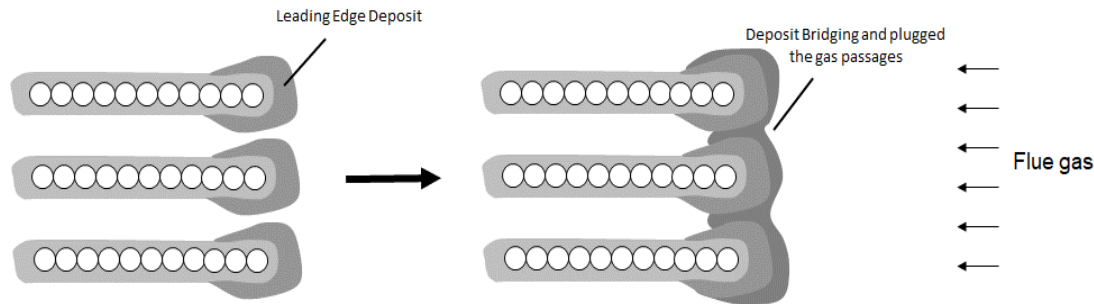
# How Pulsating & Balanced Jet is created



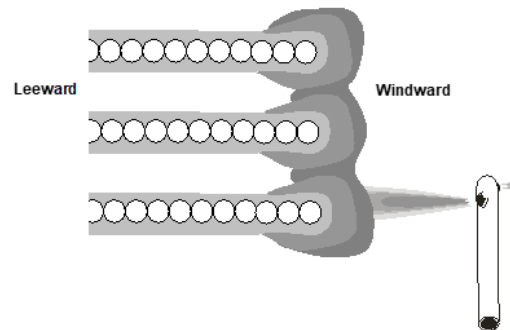


# Leading Edge Nozzle

- Plugging in a recovery boiler superheater starts with the accumulation of leading-edge deposits



- Difficult to remove leading edge deposits with direct jet impingement

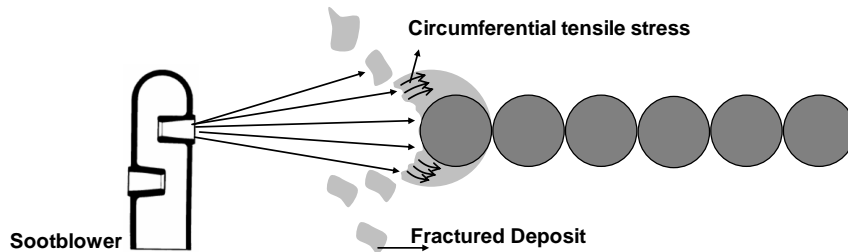




# Leading Edge Nozzle

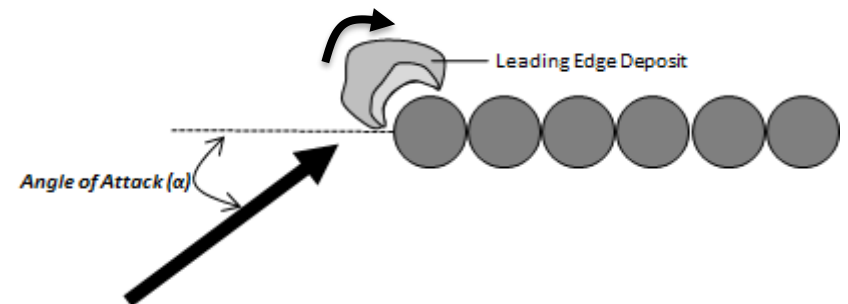
- In superheater where  $T_{\text{deposit}} > 350\text{ }^{\circ}\text{C}$ 
  - $S_{\text{adhesion ("glue")}} \lll S_{\text{Deposit tensile}}$
  - Easier to remove the leading edge deposit by debonding (*breaking the “glue” between the deposit/tube*) instead of brittle breakup (*breaking the actual hard-solid deposit itself*)

## Brittle Break-up



*Difficult to remove due to high  $S_{\text{tensile}}$   
Need high pressure and sharp jet to break the  
deposit (can also damage the boiler tubes)*

## Debonding



*Easier to remove because  $S_{\text{adhesion}} \lll S_{\text{tensile}}$*



# Leading Edge Nozzle

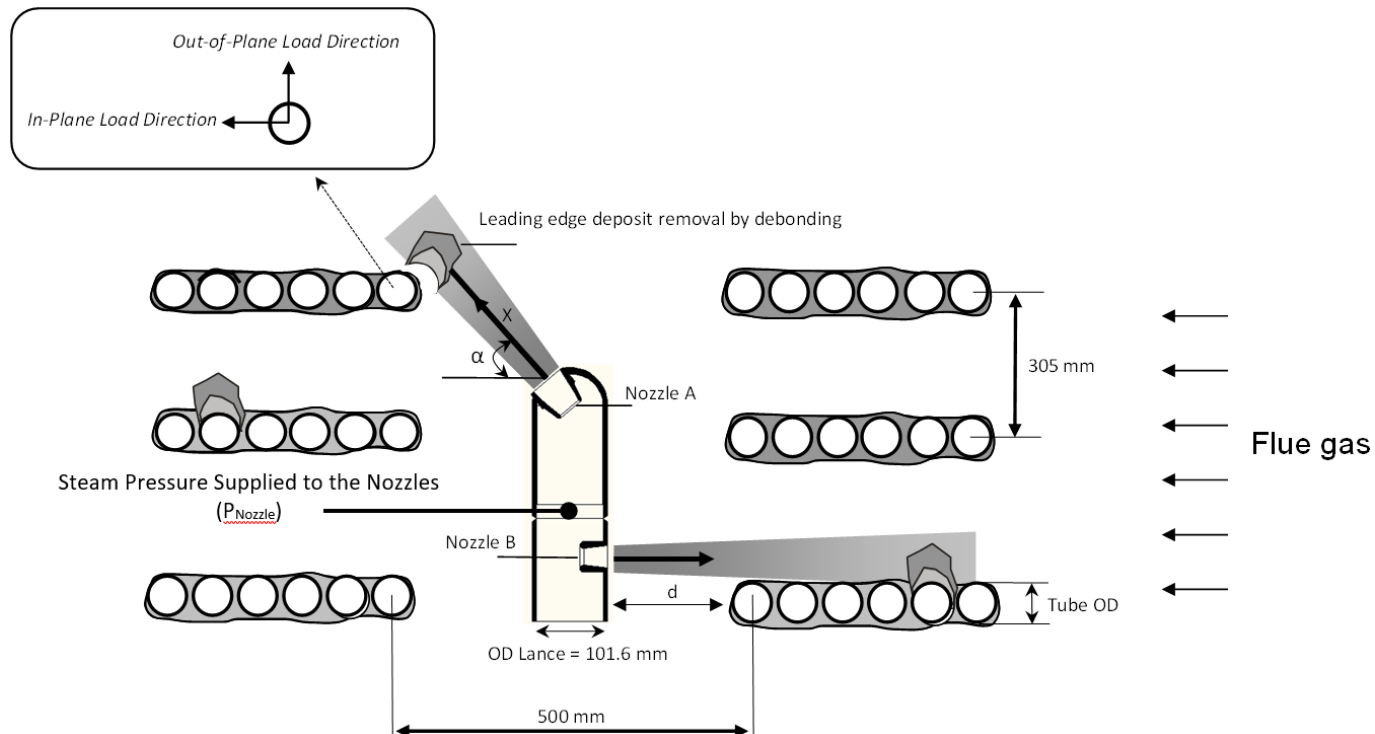
TAPPI PEERS 2020  
Session 11

## THE IMPACT OF UTILIZING THE LEADING EDGE SOOTBLOWER NOZZLE ON RECOVERY BOILER SUPERHEATER PLATENS

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University of Toronto

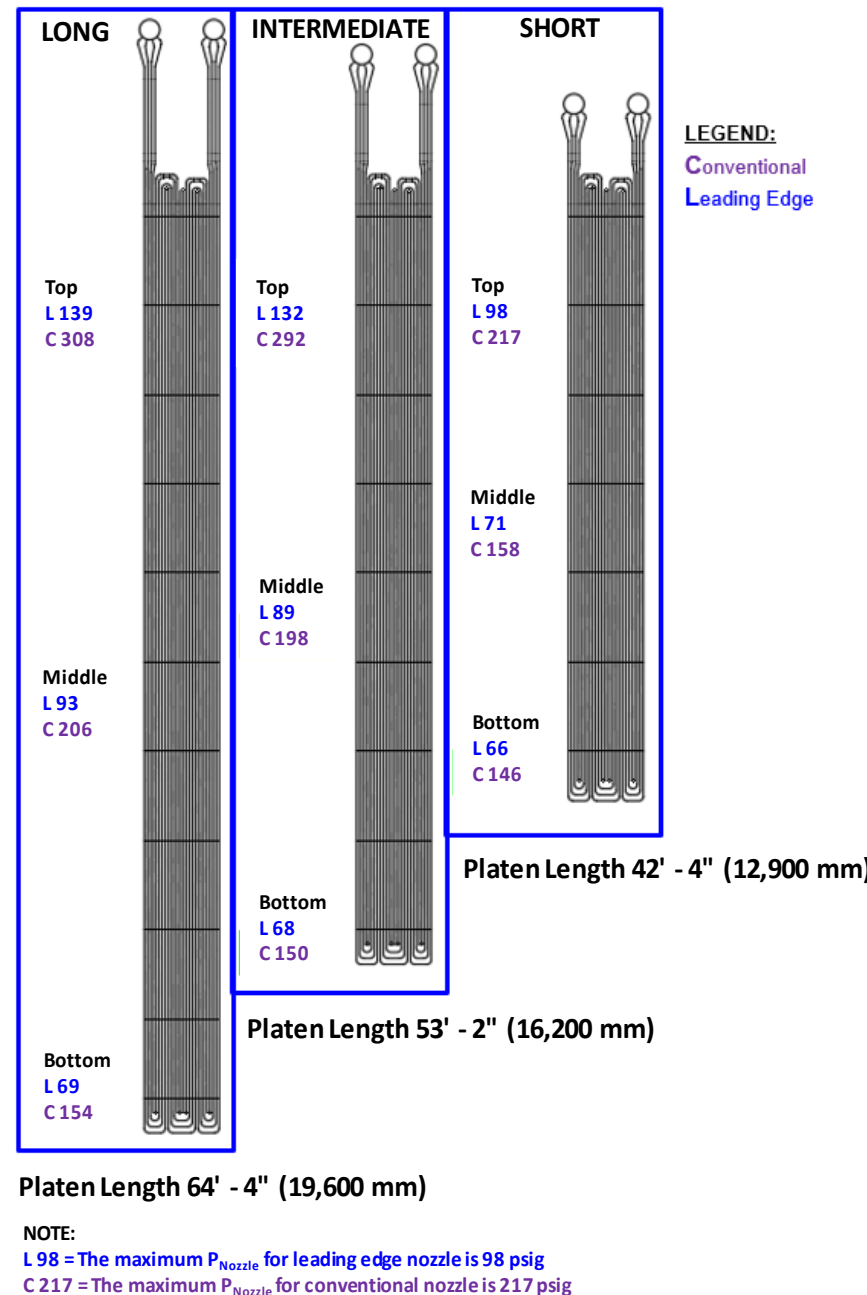




# Guideline

## TAPPI PEERS 2020

- Effective in dealing with heavy fouling & plugging
- May improve the boiler runtime
- However, there is a concern that it may damage the boiler tube if used inappropriately.
- Ongoing study with the University of Toronto.

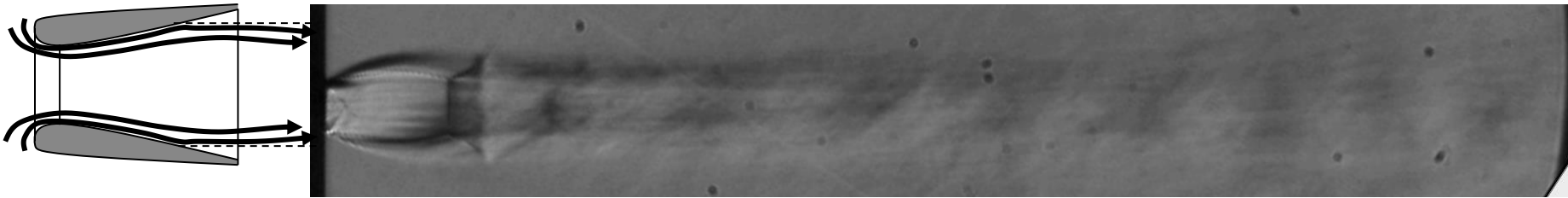




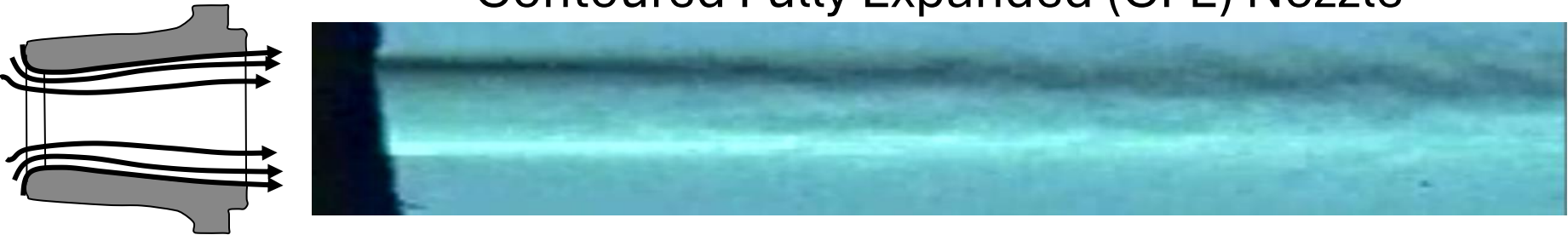


# Fully Expanded Nozzle

## Conventional Underexpanded Nozzle



## Contoured Fully Expanded (CFE) Nozzle



- Fully Expanded Nozzle is defined as a nozzle that can fully expand the  $P_{\text{Nozzle}}$  to the ambient pressure inside the boiler, thereby, converting the steam pressure completely into velocity, and prevent the formation of shock wave.



# Deposit Removal

## Three Objectives

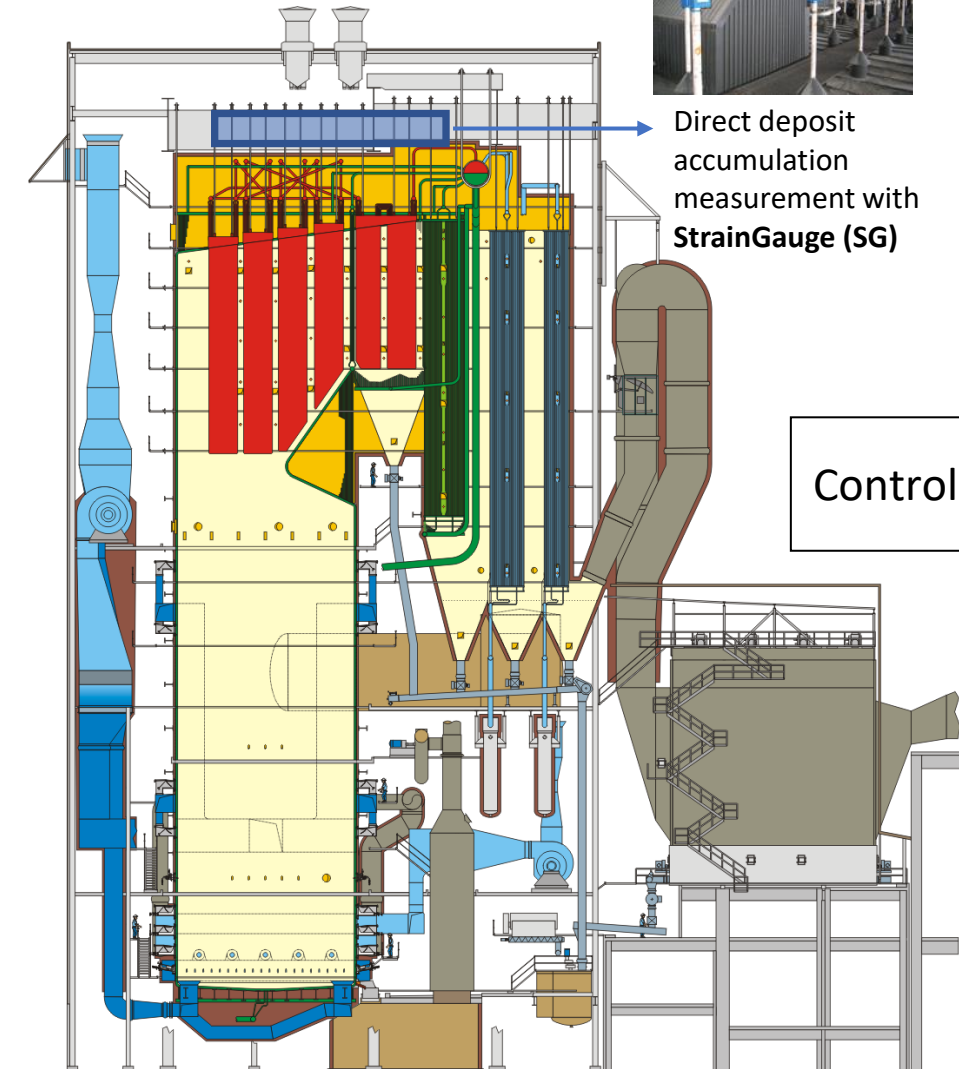
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## Technology Development

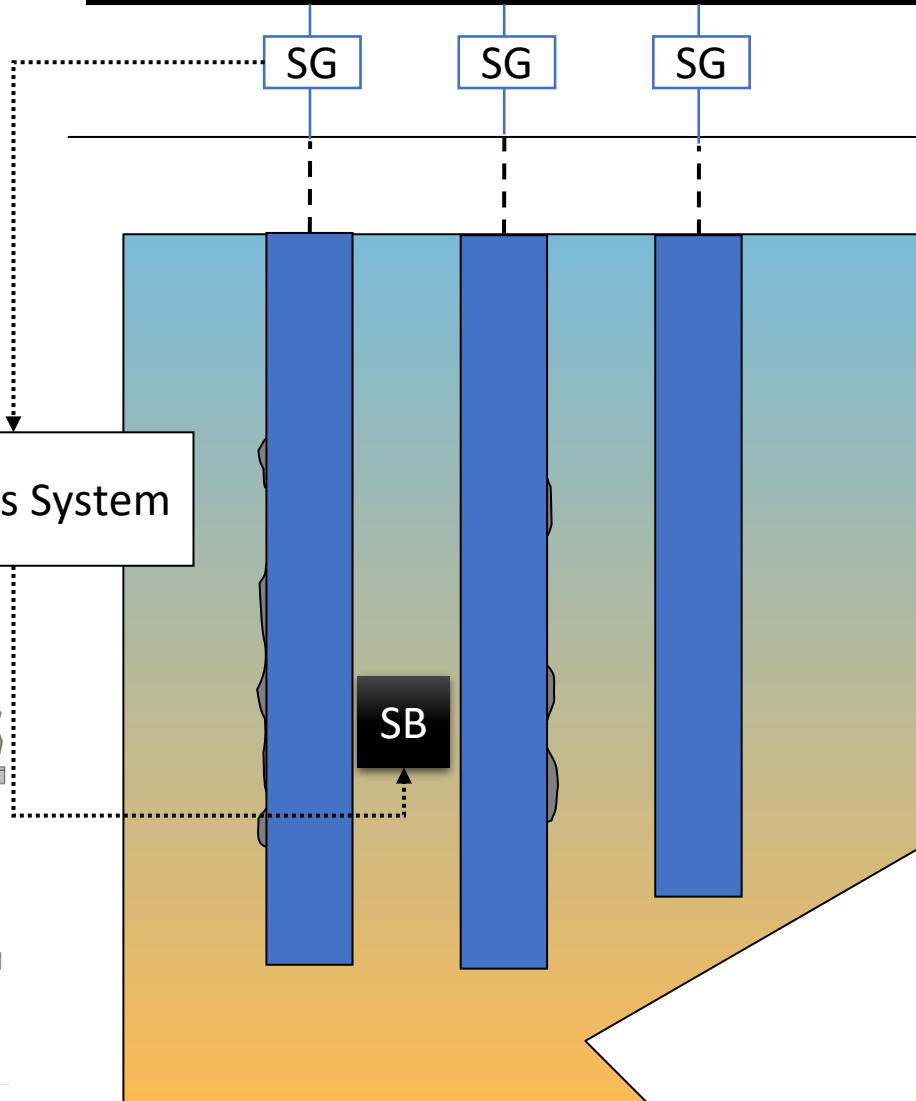
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# Targeted / Intelligent Sootblowing



Controls System





# Zero Cooling Flow

- The steam used for sootblowing also acts as a coolant to prevent the lance tube from overheating.
- If a sootblower is located in non-critical area and the lance material & design allow for one-way blowing operation, it is desirable to lower the cooling flow to save steam but not too low so as to cause lance tube overheating.

*Active US Patent – International Paper  
Andrew K. Jones*



# Zero Cooling Flow



*Active US Patent – Andrew K. Jones*

Stationary IR sensor can be used to monitor the skin temperature of the lance and adjust the cooling flow accordingly to prevent its lance tube and/or the neighboring lance tubes from overheating

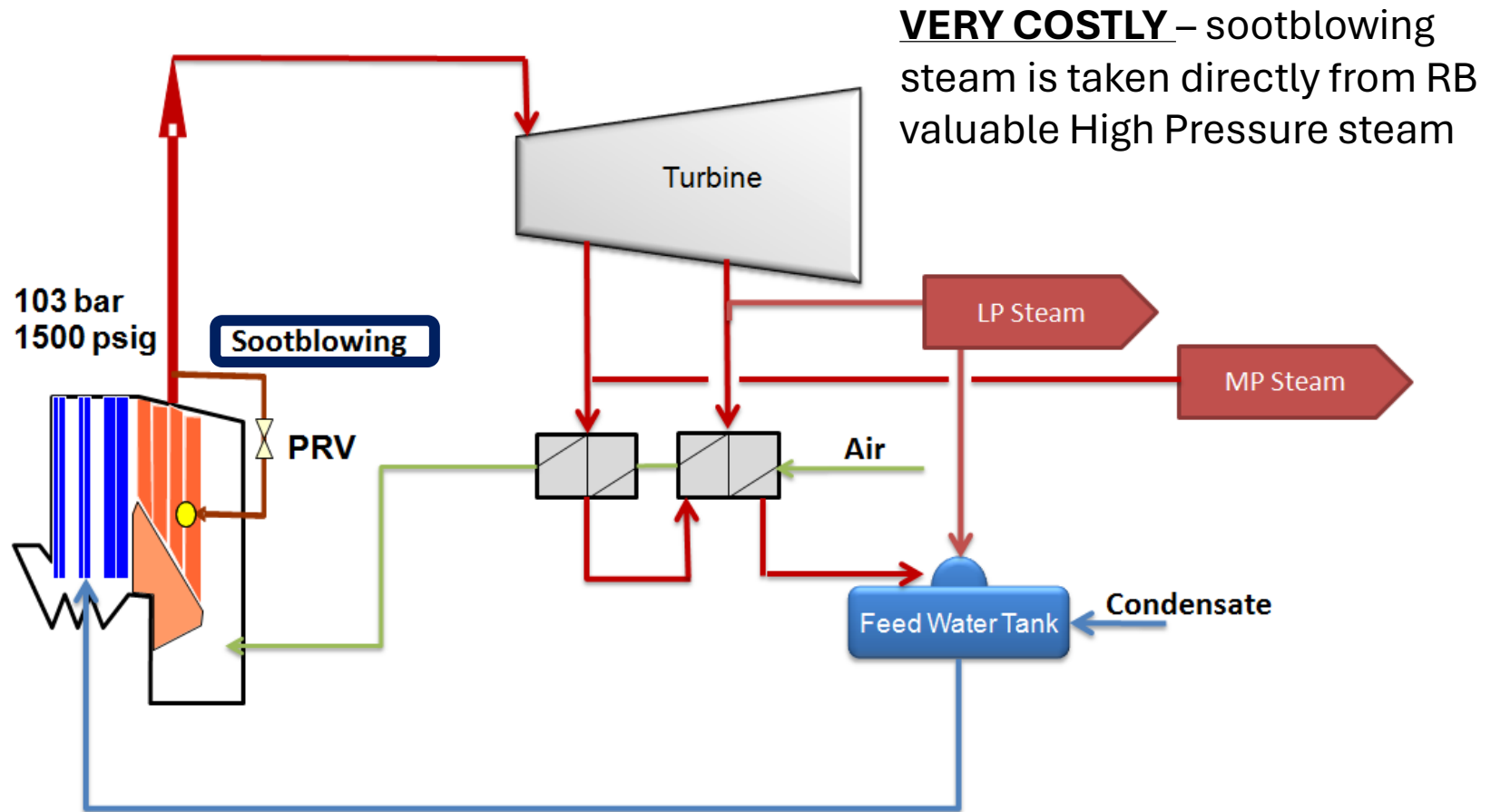


# 9-14 bar low pressure sootblowing

- **Best Available Tech:**
  - Allow more MW Generation
  - For a new recovery boiler project, this technology most definitely provides the best ROI.

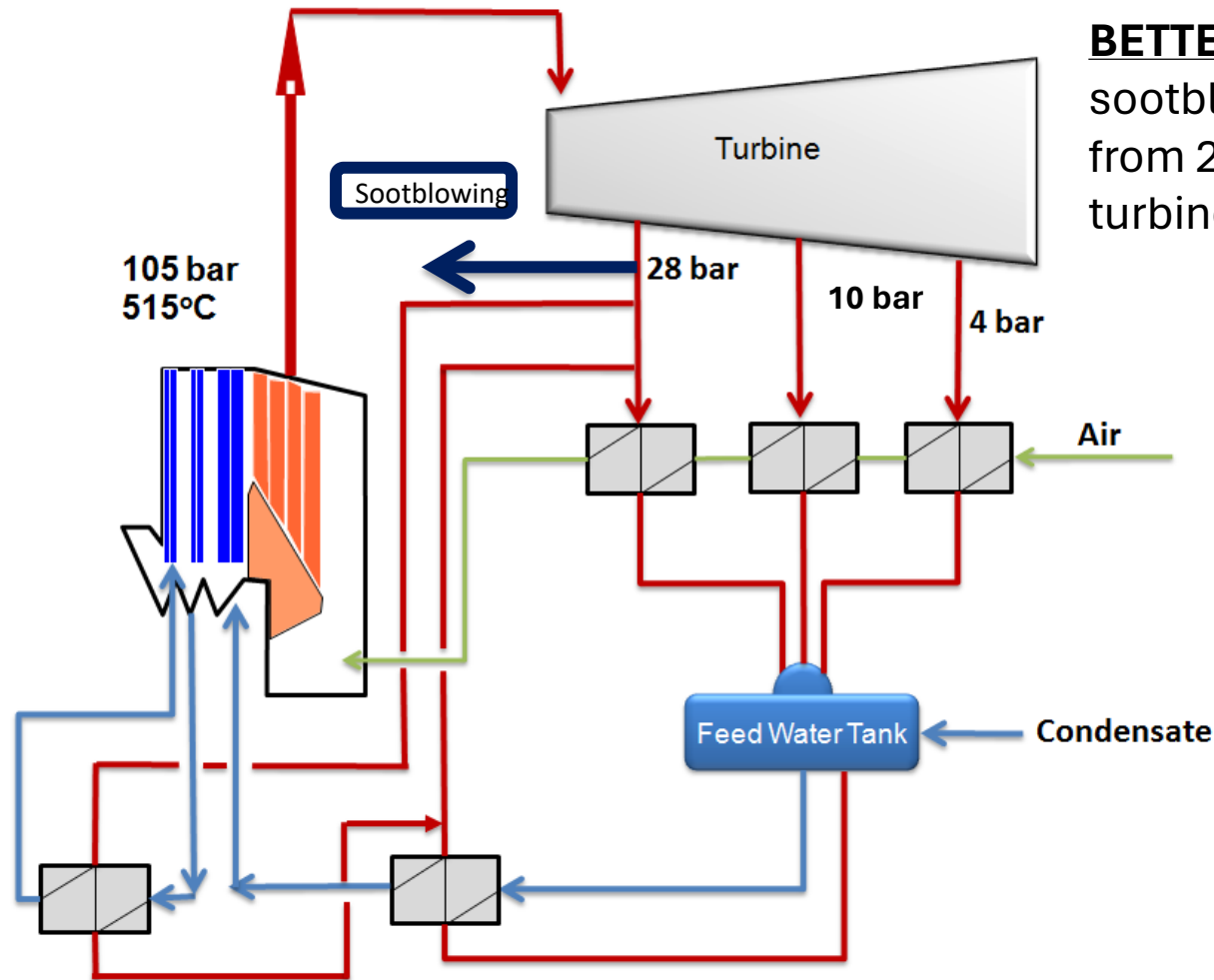


# Old Tech: Sootblowing 20+ years ago





# Conventional Sootblowing



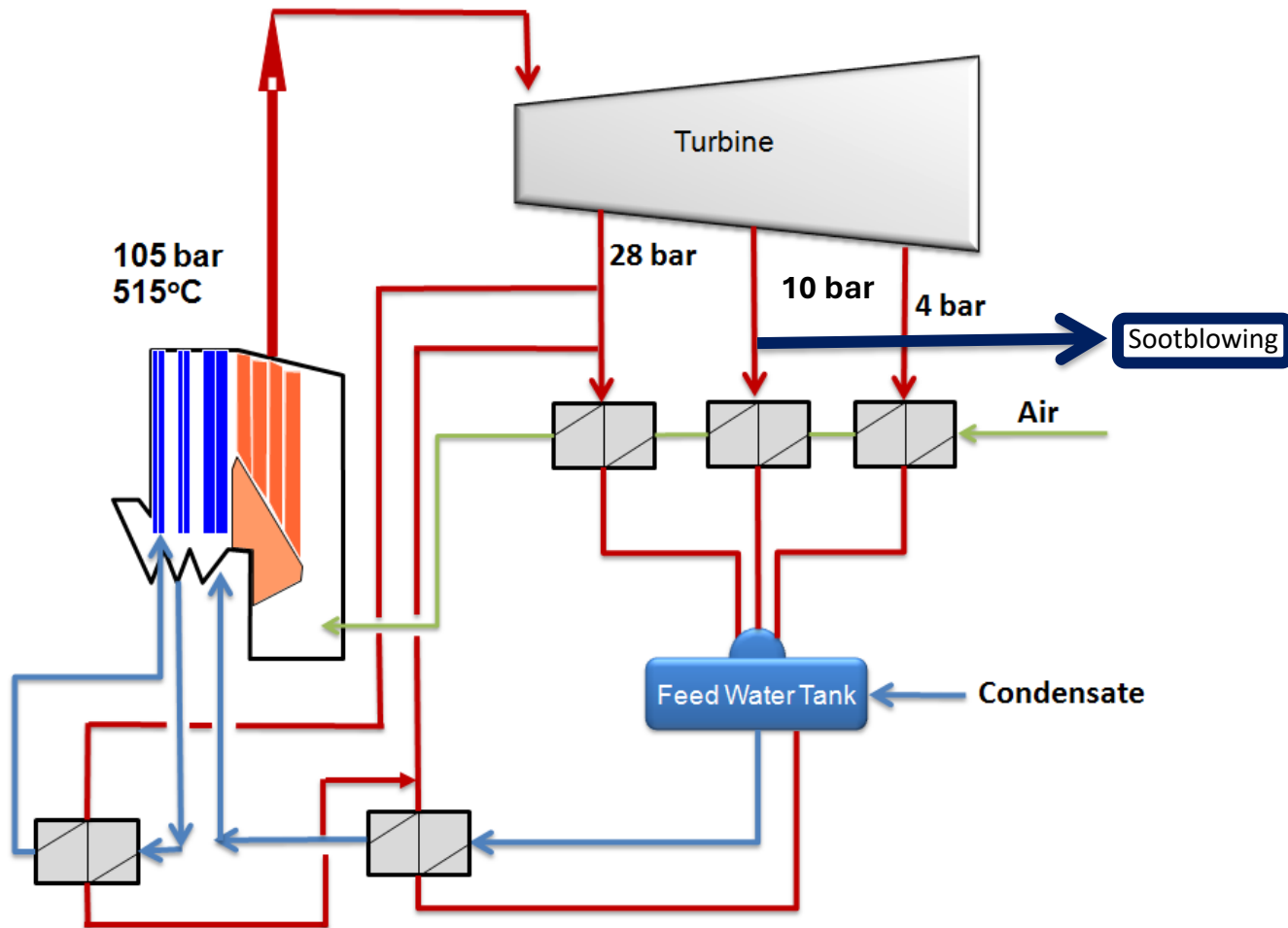
## **BETTER BUT STILL COSTLY**

sootblowing steam is taken  
from 28 bar g (400 psig)  
turbine extraction



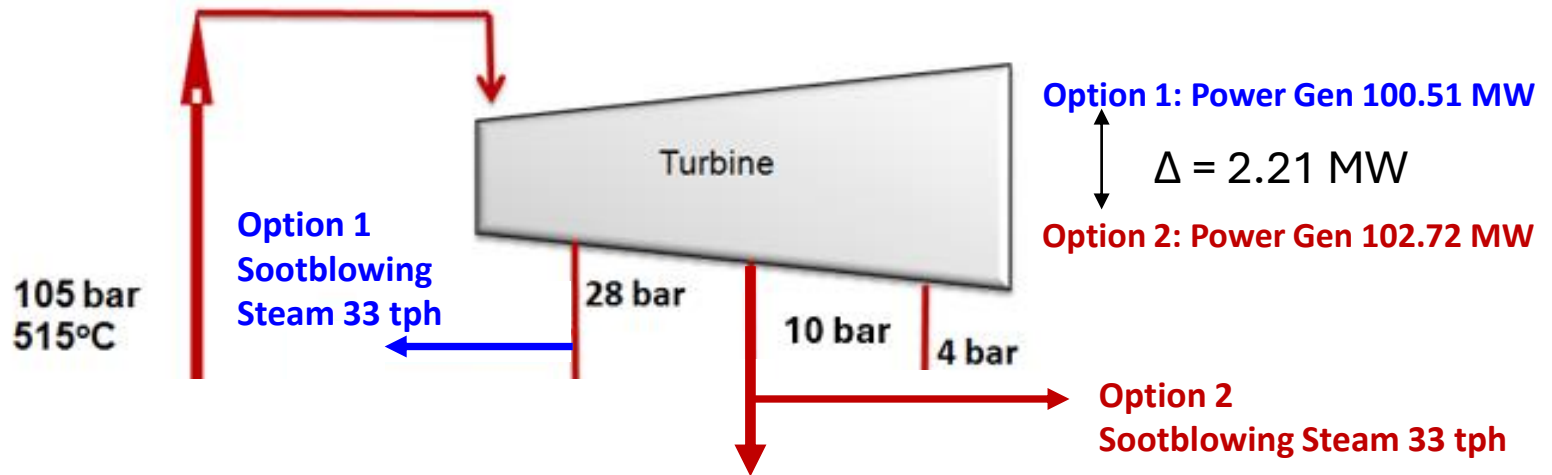


# Best Technology: 9 – 14 bar sootblowing





# Comparison

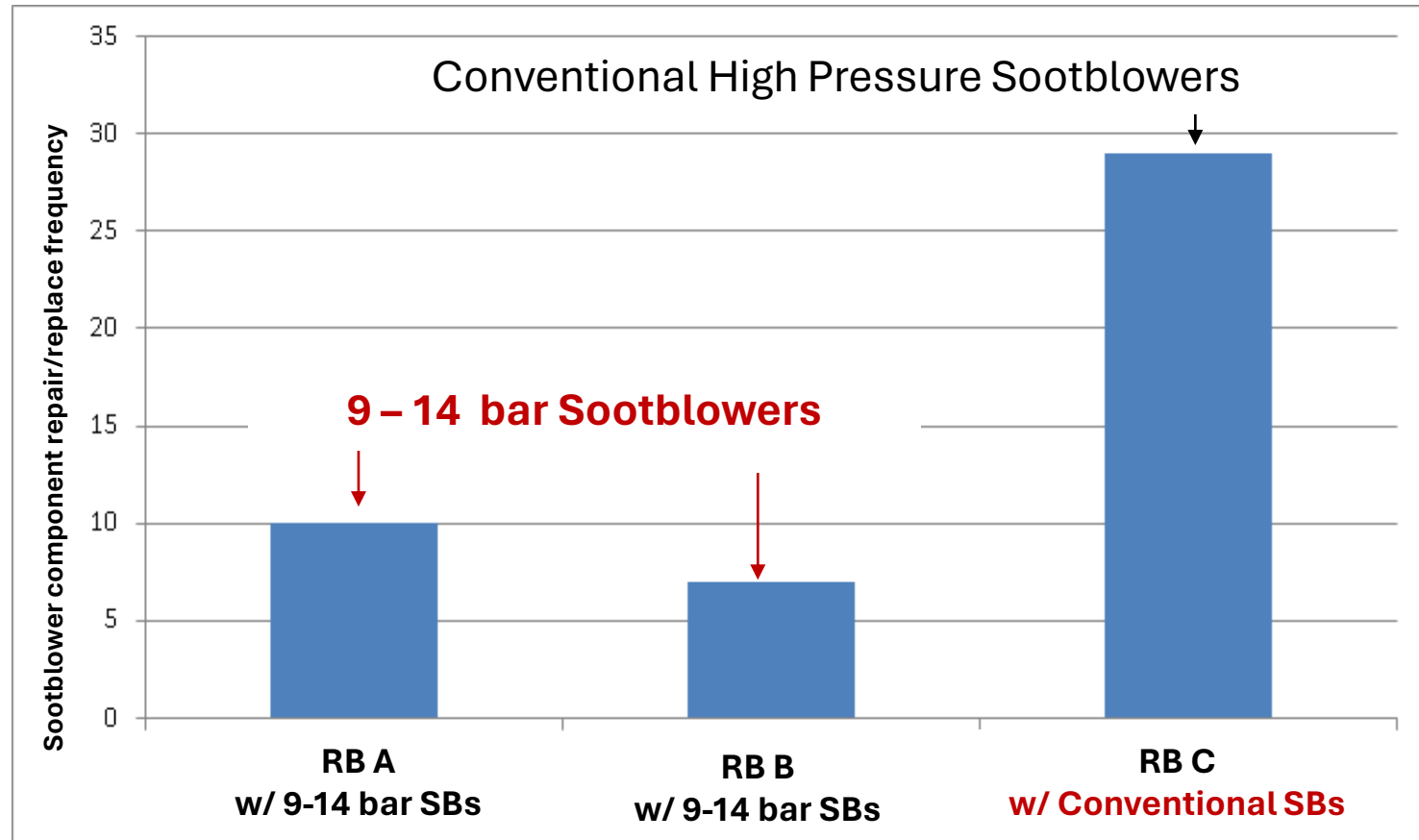


- For 33 ton/hr steam consumption, the mill can generate additional 2.21 MW with Option 2
- If the cost of energy is assumed to be € 100 / MWh, the saving per year is estimated about €2M *(assuming 355 operation days per year)*

$$2.21 \text{ MW} \frac{\text{€}100}{\text{MWh}} 24 \text{ hr } 355 \text{ days} = \text{€}1.9 \text{ M/yr}$$



# Other benefit: Lower Maintenance Costs



- The wear and tear components, such as *packing and poppet valve*, of the 9-14 bar sootblower has longer service life than its High Pressure sootblower counterpart. This may be due to lower operating pressure experienced by the 9-14 bar sootblower.



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# Summary

- Three objectives
  - Don't plug & damage my boiler
  - Don't waste my steam
  - Keep it safe & reliable
- Nozzle tech has reached its maturity, with the exception of the leading edge nozzle where ongoing research is underway to improve the advantages and minimize the downsides
- Targeting / Intelligent Sootblowing and 9-14 bar low pressure sootblowing provide the best available technology to save energy



# BACK UP SLIDES



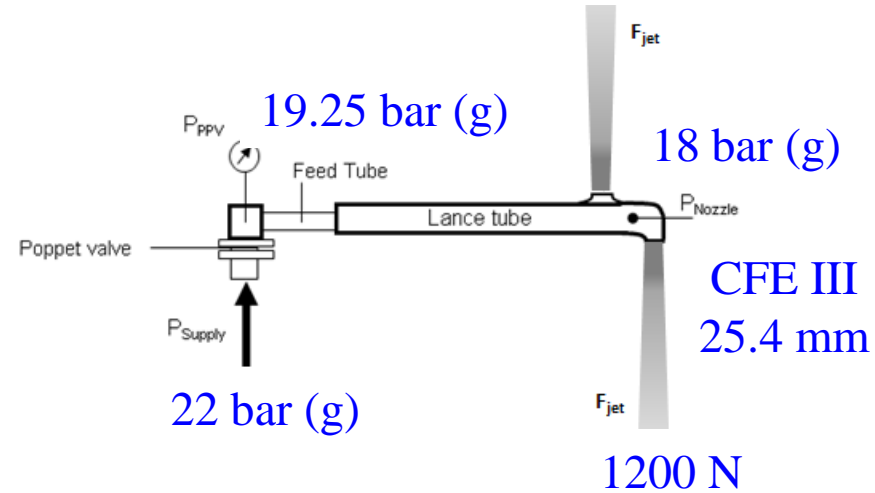
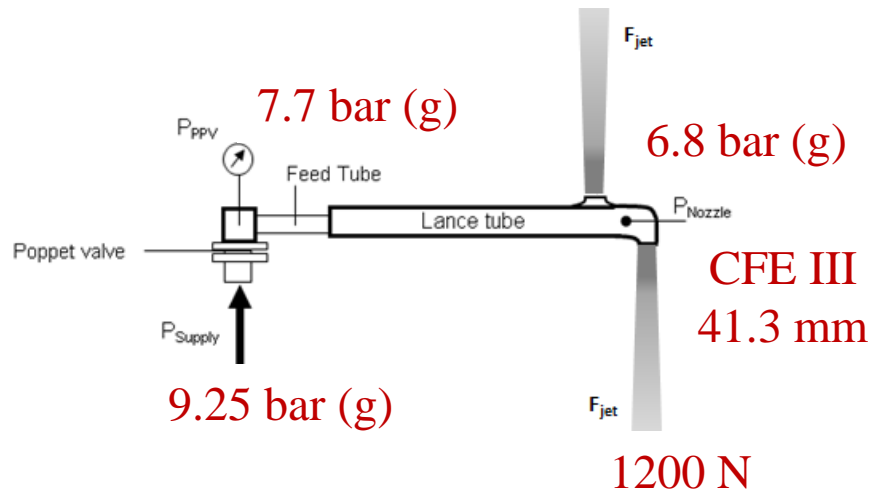
# Sootblower Design: Basic Principles

Content	%Cl At BLDS	% K At BLDS	Required Cleaning Force
Very Low	< 0.1	< 0.7	800 N
Low	0.1 – 0.3	0.7 – 1	900 N
Typical	0.3 – 0.7	1 – 2	1050 N
High	0.7 – 2.5	2 – 4	1200 N

- Sootblower should be designed with the worst case scenario in mind, ready to combat heavy fouling if needed
  - Clyde Industries recommends the sootblowers to be designed with the capability to increase the cleaning force to 1200 N **to deal with possible boiler upset and heavy fouling**
-



# Deposit Removal Criteria



$$F_{\text{jet}} (41.3\text{mm}) = F_{\text{jet}} (25.4\text{mm})$$

$$P_{32\text{mm}} * \text{Impact Area}_{41.3\text{ mm}} = P_{25.4\text{mm}} * \text{Impact Area}_{25.4\text{mm}}$$

$$0.68 \left( \frac{N}{\text{mm}^2} \right) \frac{1}{4} \pi (41.3)^2 \text{ mm}^2 = 1.8 \left( \frac{N}{\text{mm}^2} \right) \frac{1}{4} \pi (25.4)^2 \text{ mm}^2$$

6.8 bar

Note that the above equation is the simplified version of the physic of the jet dynamics

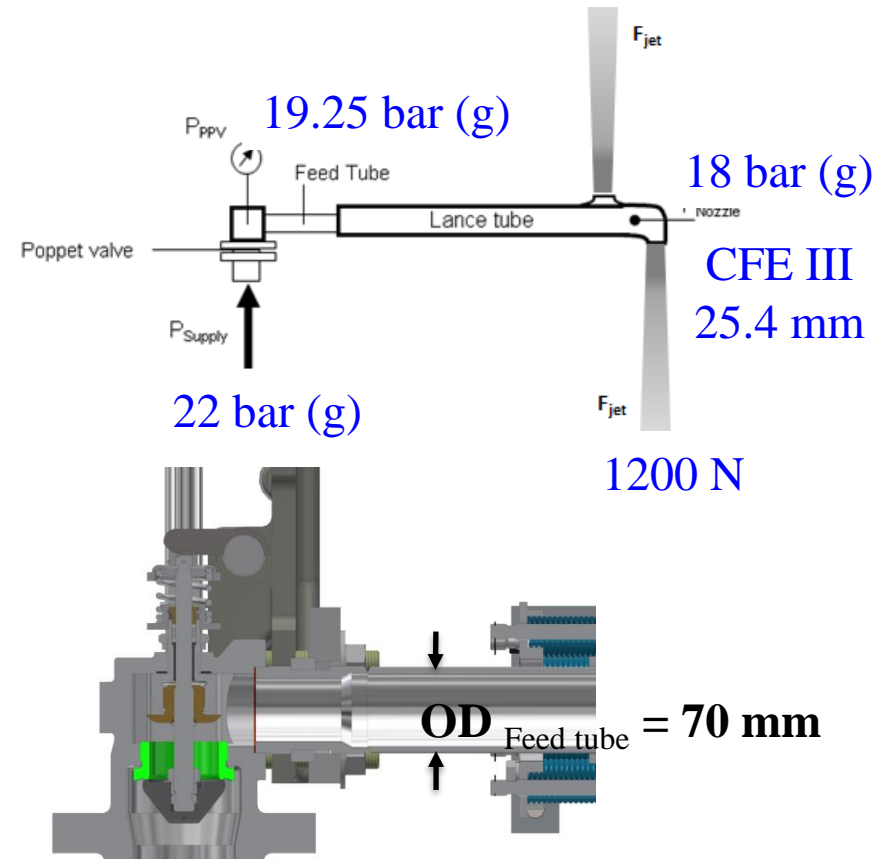
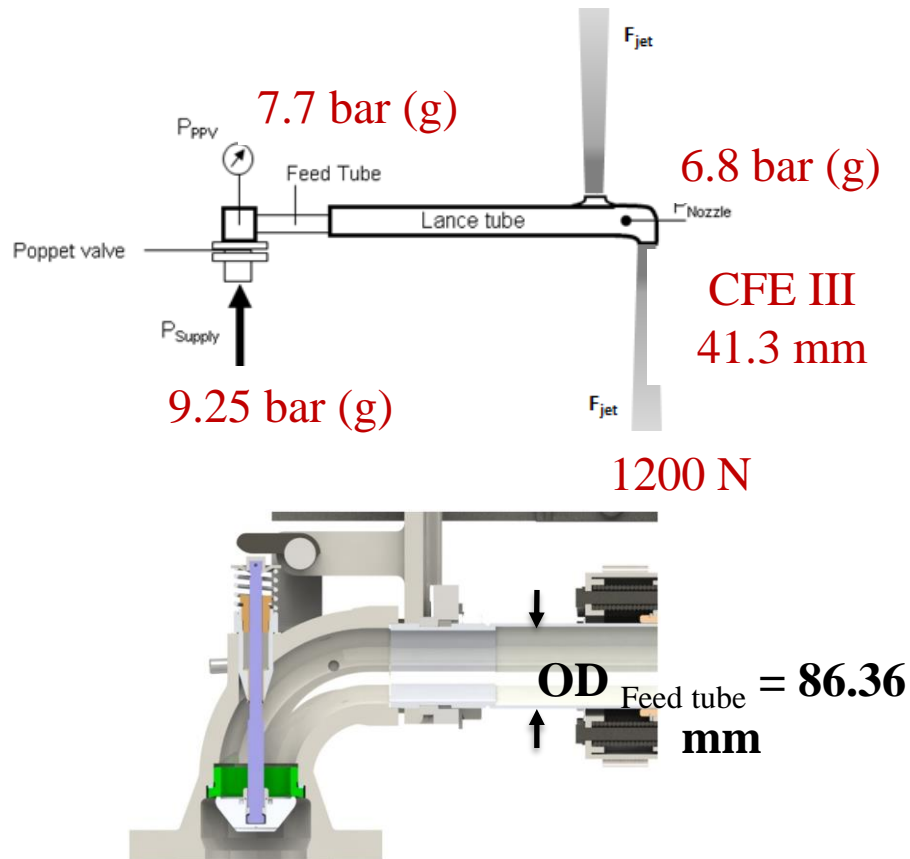
NOT TO BE USED TO DESIGN THE SOOTBLOWER

18 bar





# Deposit Removal Criteria

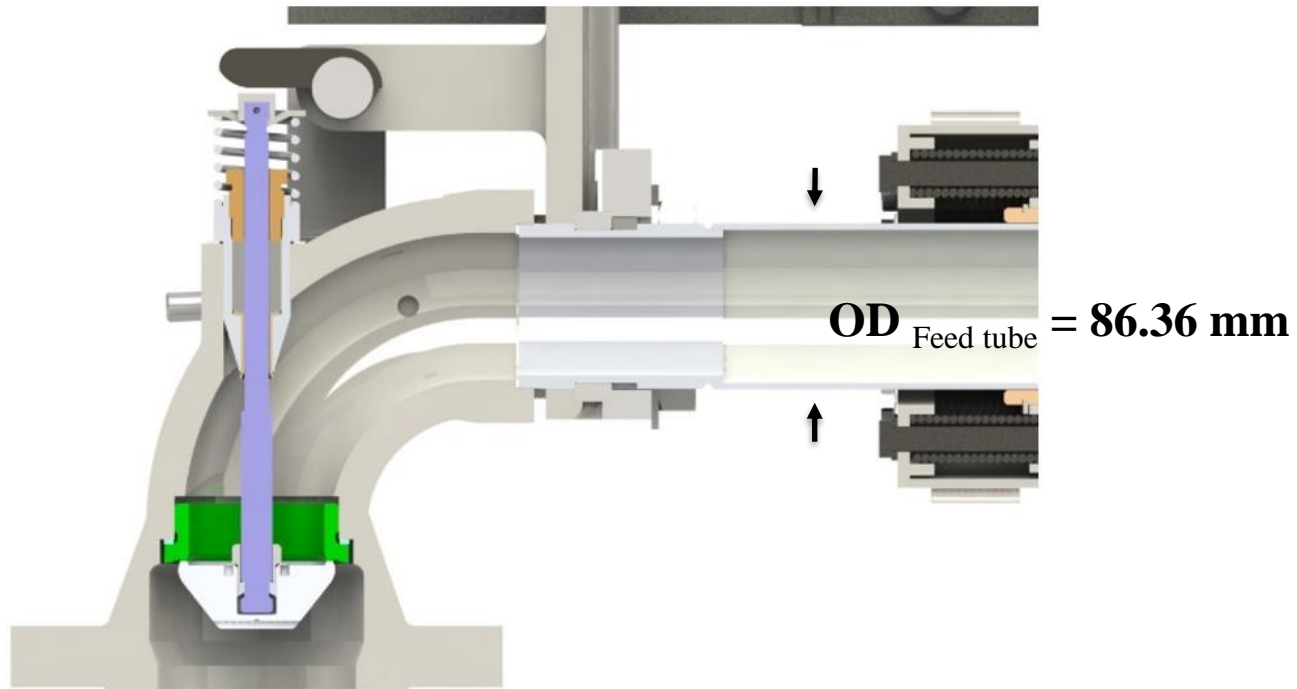


*Lower  $P_{Supply}$  is possible with low pressure drop sootblower*



# 9 – 14 bar Sootblower: Poppet Valve

- Elbow-like poppet valve to minimize costly pressure drop





SUOMEN SOODAKATTILAYHDISTYS  
FINNISH RECOVERY BOILER COMMITTEE



# Introduction to Sootblower Nozzle

*May 2023*





How about the steam consumption?

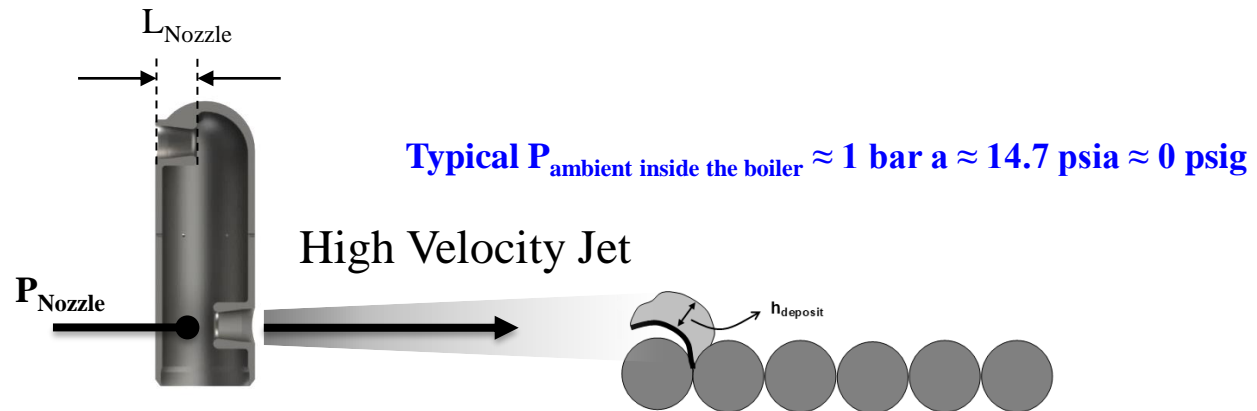
Does **low pressure** consume more steam than **high pressure**?

*No, it does NOT*





# Ideal Nozzle



- The main function of a sootblower nozzle is to convert high pressure steam supplied to the nozzle ( $P_{\text{Nozzle}}$ ) to high velocity jet.
  - An ideal nozzle is defined as a nozzle that can fully expand the  $P_{\text{Nozzle}}$  to the ambient pressure inside the boiler, thereby, converting the steam pressure completely into velocity (i.e., 100% efficiency).
  - A fully expanded nozzle is a nozzle with 100% nozzle efficiency
-

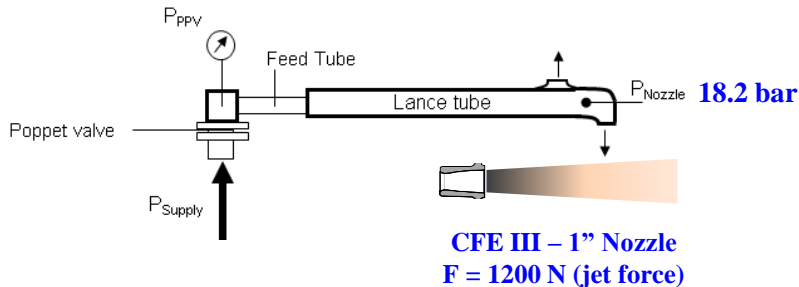


# Comparison

## CFE III – 25.4 mm (1”) throat diameter



Flow Rate through both nozzles = 2.43 kg/s

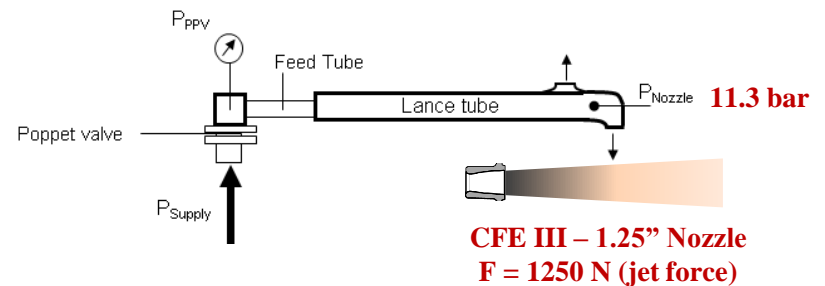


- Require 18.2 bar at the nozzle and steam flow rate of 2.43 kg/s to produce 1200 N

## CFE III – 32 mm (1.25”) throat diameter



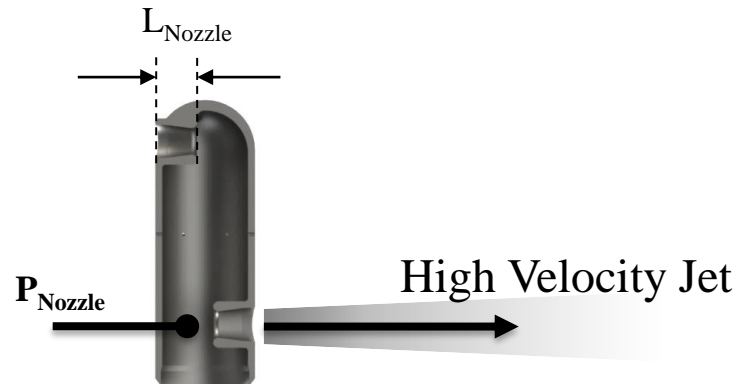
Flow Rate through both nozzles = 2.43 kg/s



- CFE III – 1.25” nozzle is more efficient than its 1” counterpart. It produces higher cleaning force of 1250 N and requires only 11.3 bar at the nozzle and the same flow rate of 2.43 kg/s



# Why CFE III – 1.25” is more efficient than 1”



- The higher the  $P_{\text{Nozzle}}$ , the longer  $L_{\text{nozzle}}$  (nozzle length) must be designed to fully expand the  $P_{\text{Nozzle}}$ .
- Unfortunately, the  $L_{\text{nozzle}}$  is restricted to the lance OD (which is typically 3.5” or 4”)
- CFE III – 1.25” is more efficient than its 1” counterpart because it only need to expand the steam pressure from 11.3 bar (compared to 18.2 bar for CFE III – 1”) to 1 bar ambient pressure.
- Hence the  $L_{\text{nozzle}}$  requirement to fully expand the  $P_{\text{Nozzle}}$  doesn't have to be compromised by cutting it short (like the CFE III - 1”) to fit the nozzle into the lance OD.
- Therefore, Clyde Industries has standardized its nozzle offering to a more efficient CFE III – 1.25”